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# Waste Heat to Power

# Selecting a Technology

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September 25, 2007

# **Presentation Outline**

**Overview of Waste/Reject Heat in Industrial Processes** 

- > Refining
- Petrochemical
- Inorganic chemicals
- Process Steam
- Engine exhaust

#### **Technologies for Waste Heat to Power Conversion**

- Commercial Technologies
- Emerging Technologies

**Technology Merits** 

- > Conversion efficiency and effective utilization of waste heat
- Heat transfer equipment
- System integration and interfacing with industrial processes
- System reliability
- Economic values

#### Selecting a Technology

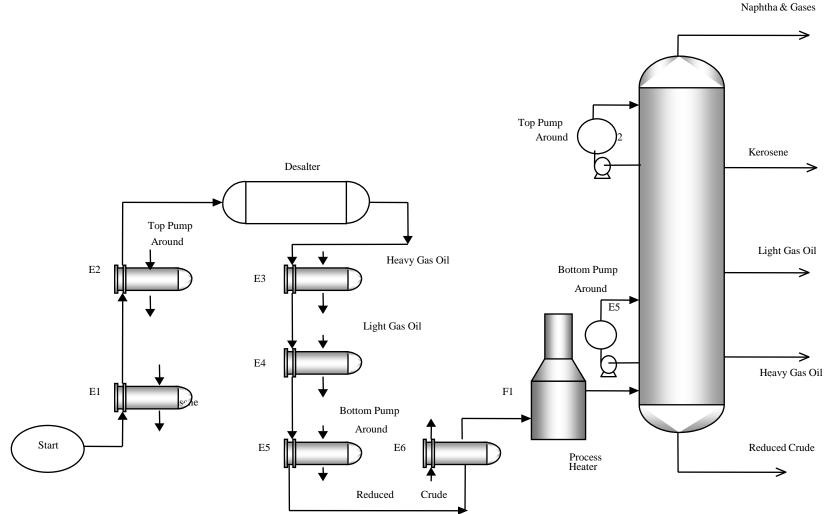
**Perspectives on Waste Heat Recovery and Utilization** 



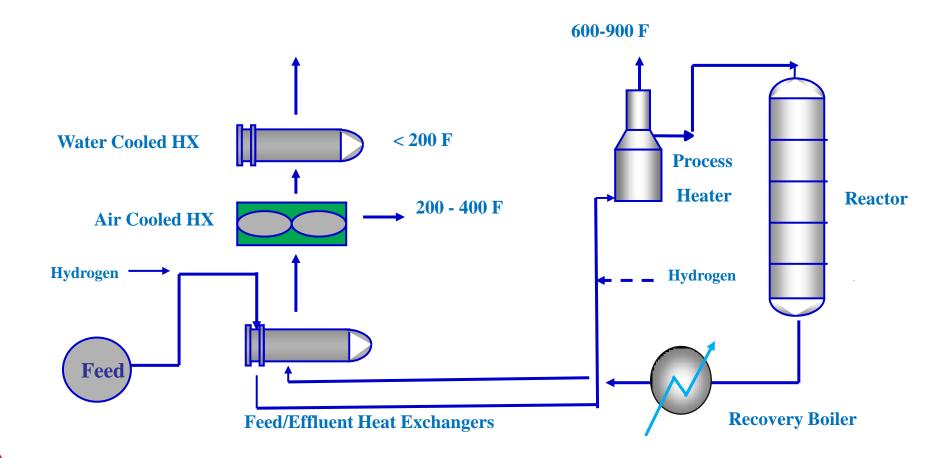
# Energy Consumption in a Typical Refinery

| Energy consumption in a typic                    | cal refinery is 441,000 B | tu/bbl crude, most |
|--|---------------------------|--------------------|
| of which must be rejected to t                   | he atmosphere or coolir   | ng water           |
| Process heaters and steam boilers (600F – 800F+) |                           | 87,000 Btu/bbl     |
| Process heat (200F – 400F)                       |                           | 40,000 Btu/bbl     |
| Process heat (< 200F) to cooling water           |                           | Remaining          |
|  | Average                   | US Energy Use      |
|  | KBtu/bbl                  | TrillionBtu/Year   |
| Crude distillation                               | 205.3                     | 880                |
| Delayed coking                                   | 166.0                     | 101                |
| > FCC  | 100.0                     | 190                |
| Hydrotreating/Hydrocracking                      | 360.0                     | 581                |
| Reforming  | 284.0                     | 373                |

# **Crude Distillation Major Energy Consuming Process**

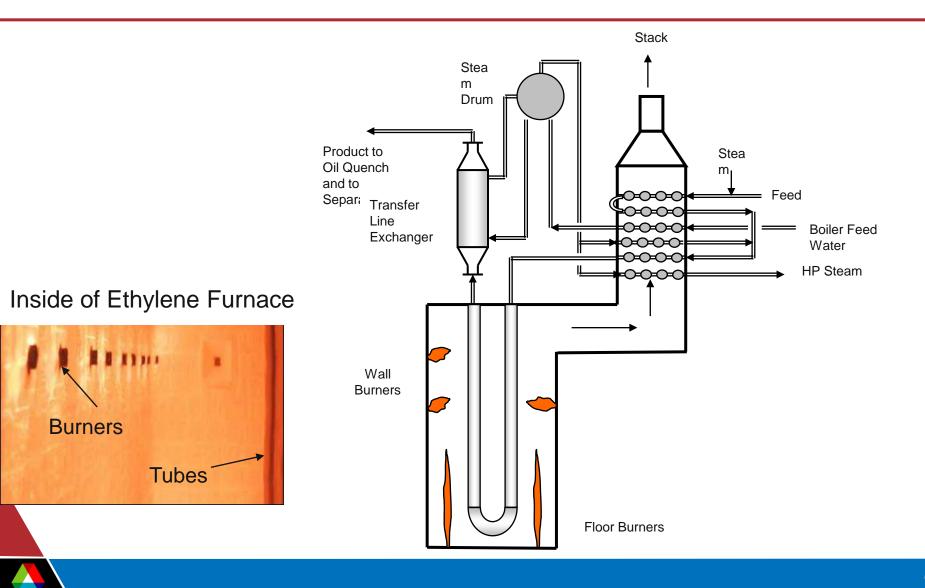


# Hydrotreating and Reforming Processes

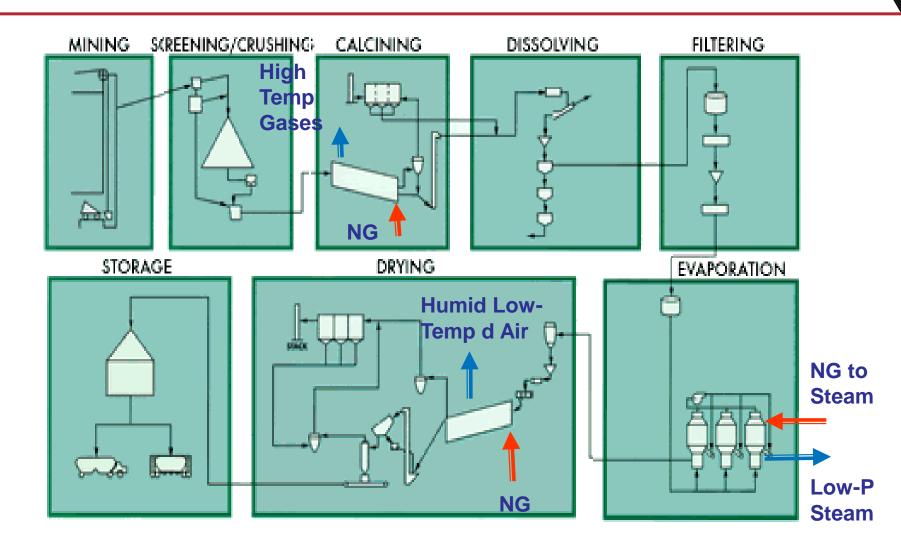


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# **Olefin Reactor – Complex Furnace Design**



# Soda Ash Process – Complex Furnace Design



# **Steam Utilization in Process Industries**

- Steam is major heat carrier in refining, petrochemical, and pulp&paper, and food processing industries
- Steam optimization is an on-going effort with commercial softwares in the market
- Cost effective topping cycle provides opportunity to improve steam economy
- Effective utilization of low-pressure steam can significantly
  - improve the overall steam economy and plant energy efficiency

## **Current Practices of Heat Recovery**

Heat recovery is generally considered in the process design optimization

- Feed/effluent heat exchangers to recover high-level heat
- Waste heat recovery boilers for high-pressure steam generation
- Fired-heater stack gas heat recovery for preheating combustion air

## **Current Practices of Heat Rejection in the Process Industry**

Heat rejection is generally not considered in the process design optimization

- Air-cooled heat exchangers to reject medium-level (200F to 400F) heat
- Cooling water to reject low-level heat (< 200 F)</p>
  - Cooling tower (1000+ lb of water consumed per million Btu heat rejected)
  - Once through river, seawater, and lakes (environmental restrictions)

Regional scarcity of cooling water needs to be taken into consideration for waste heat to power.



# **Technologies for Waste Heat to Power**

### **Commercial Technologies**

- Single Fluid Rankine Cycle
  - Steam cycle
  - Hydrocarbons
  - Ammonia
- Binary/Mixed Fluid Cycle
  - Ammonia/water absorption cycle
  - Mixed-hydrocarbon cycle

### **Emerging Technologies**

- Supercritical CO2 Brayton Cycle
- Thermoelectric conversion

## **Combined Cycles**

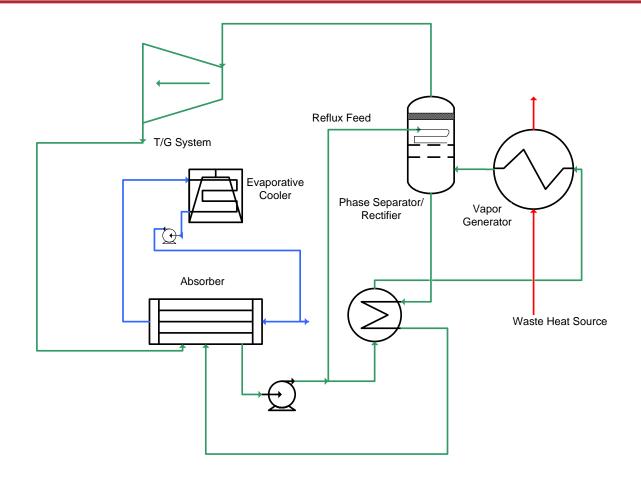
# **Rankine Cycle**

- Steam Cycle
  - High temperatures
  - Waste heat-recovery boilers commonly used
  - High-pressure steam used for large compressors and air blowers
- Hydrocarbons Cycle (Organic Rankine Cycle)
  - Medium to high temperatures
  - Developed for geothermal applications
  - Diesel engine exhaust DOE project on ORC
- Ammonia
  - Low temperatures
  - Developed for ocean thermal energy
  - Bottoming cycle with potential dry cooling

Ammonia/Water Absorption Power Cycle Historical Perspectives

- Ammonia/water absorption cycle is commercially used for heat-activated refrigeration
- Ammonia absorption power system proposed in 1981 by H. Sheets for ocean thermal energy
- First patented as Kalina cycle in 1982, followed by publication in 1984
- In 1999-2000 first commercial scale 2.0 MW Kalina cycle plant installed at a geothermal site in Iceland
- Further developments continue:
  - Cycle configuration and integration for improved thermal efficiency
  - Development of heat/mass transfer equipment

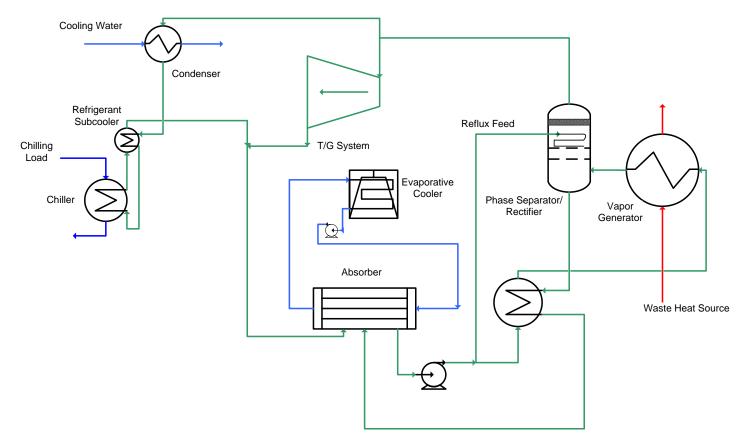
# Ammonia/Water Absorption Power Cycle Basic Cycle



Heat recuperation within the cycle is key to high thermodynamic efficiency

### Ammonia/Water Absorption Power Cycle

### **Dual-Function Cycle for Power and/or Refrigeration**



- Dual-function cycle concept developed at Energy Concepts Company, LLC
- Power and refrigeration can be used interchangeably or simultaneously

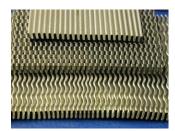
- Advancement of Organic Rankine Cycle with improved thermal efficiency
- Significant literature on cycle analysis
- Industry is familiar with the technology
- **Commercially available heat transfer equipment and turbine/generator**
- System integration No major technical risks

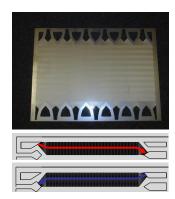


# Supercritical CO2 (SCO2) Brayton Cycle

### **Being Developed for Nuclear Plants**

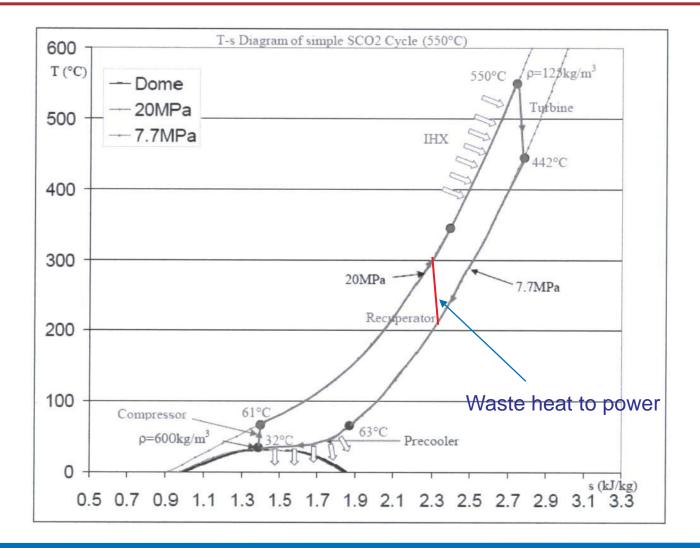
- SCO2 Brayton cycle achieves high thermal efficiency
- Development of heat transfer equipment
  - Internal heat recuperation crucial for achieving high thermal efficiency
  - Compact narrow flow passage heat exchangers
- Turbine/Compressor
  - Single-stage and two-stage centrifugal compressors
  - Six-stage axial flow turbine
- For waste heat to power applications, combined cycle may have advantages





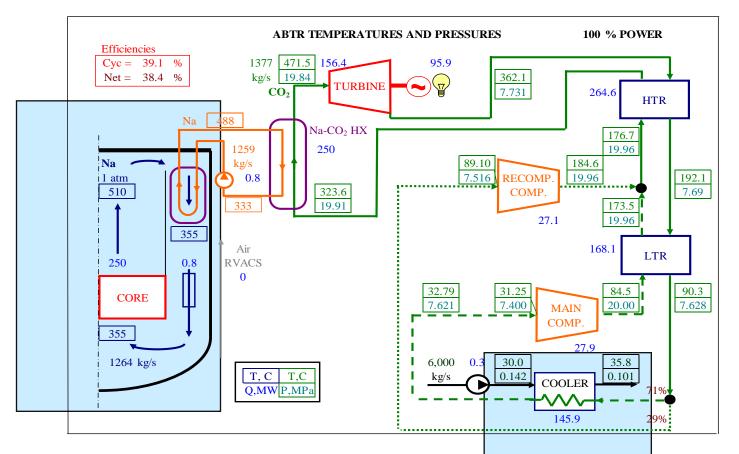


# Supercritical CO2 (SCO2) Brayton Cycle for Nuclear Reactor T-S Diagram



# Supercritical CO2 (SCO2) Brayton Cycle for Nuclear Reactor

### **Flow Schematic**

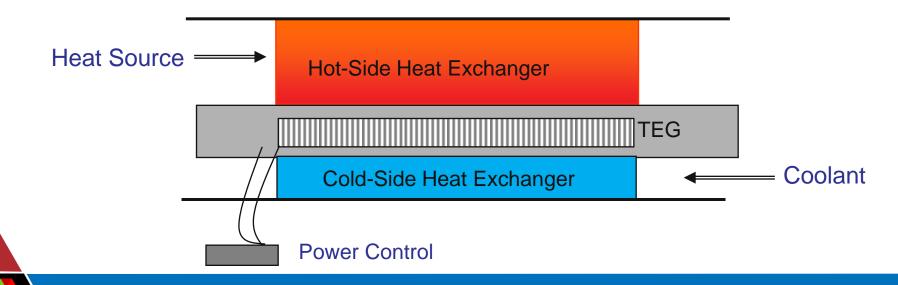


Na-Loop replaced with hot-oil loop for waste heat to power cycle

Low-temp bottoming cycle or Absorption refrigeration cycle

## **Thermo-Electric Generation System**

- Thermo-Electric Generator (TEG) device known for some time for TEG cooling (example – thermocouples)
- Development focused on material-pair with high figure-of-merit
- DOE funded project to evaluate technical/economic viability of TEG system



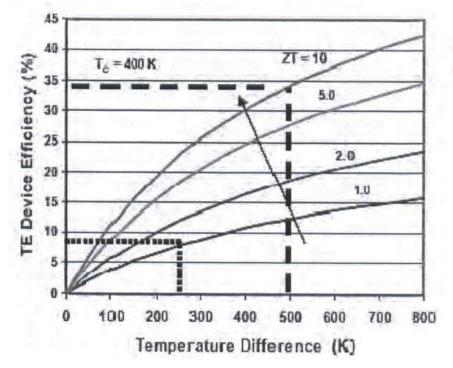
### **Thermo-Electric Generation System**

#### **Figure of Merit**

- $\mathbf{Z}\mathbf{T} = (\alpha^2 \, \sigma / \lambda \,) \, \mathbf{T}$
- $\alpha$  = the Seeback coefficient (volt/K)
- $\sigma$  = electric conductivity (amp/volt m)
- $\lambda =$  thermal conductivity (w/m K)

#### Thermal Efficiency

$$\eta_{c} = \left[\frac{T_{h} - T_{c}}{T_{h}}\right] \left[\frac{\left(1 + Z^{*}\overline{T}\right)^{1/2} - 1}{\left(1 + Z^{*}\overline{T}\right)^{1/2} + 1}\right]$$



# **Combined Cycle**

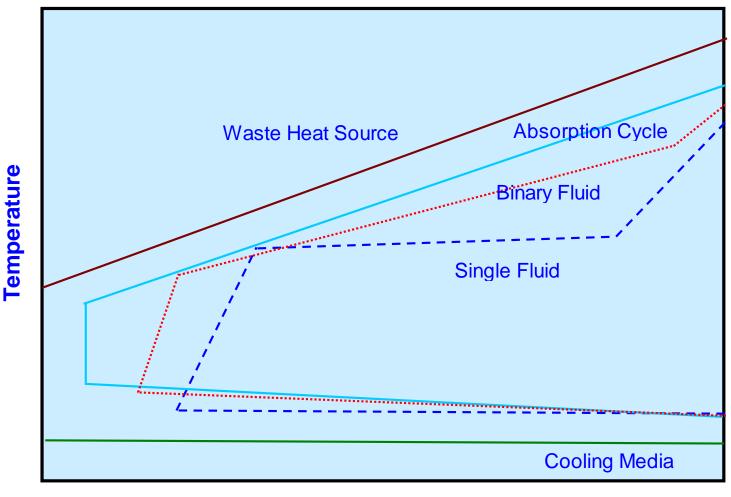
- An integrated combined cycle with advantageous features of two different cycles can be more economical than individual cycles
- Combined power and refrigeration can significantly improve the overall economics
- For an example: SCO2 and ammonia/water or organic cycle

Advantages:

- Cycle configuration
- Cost-effective interfacing with heat source
- Dry cooling
- Mitigating material issue
- Refrigeration

# **Technology Merits**

## **Conversion Efficiency and Effective Utilization of Waste Heat**





# **Conversion Efficiency and Effective Utilization of Waste Heat**

Understanding Cycle Efficiency – 1<sup>st</sup> Law of Thermodynamics

**Commercial Power Plants** 

 $\eta_c = \frac{\text{Work}_{\text{Net}}}{\text{Heat Source}}$   $\eta_c = \frac{\text{Work}_{\text{Net}}}{\text{Heat Content of Primary Soure}}$ 

Commonly thermal efficiency is based on recovered waste heat

$$\eta_{WH} = \frac{\text{Work}_{\text{Net}}}{\text{Heat Recovered}}$$

Thermal efficiency should be based on total recoverable waste heat

 $\eta_{WH} = \frac{\text{Work}_{\text{Net}}}{\text{Total Recoverable Heat}}$ 

## **Conversion Efficiency and Effective Utilization of Waste Heat**

Understanding Cycle Efficiency – 2<sup>nd</sup> Law of Thermodynamics

**Carnot Efficiency** 

$$\eta_c = \frac{\text{Work}_{\text{Net}}}{\text{Heat Source}} \qquad \eta_c = \frac{T_1 - T_2}{T_1}$$

**Cornot Efficiency for Waste heat to Power** 

$$\eta_{\scriptscriptstyle WH} = \frac{T_{\scriptscriptstyle HeatSource} - T_{\scriptscriptstyle {\rm Re\,jection}}}{T_{\scriptscriptstyle HeatSource}}$$

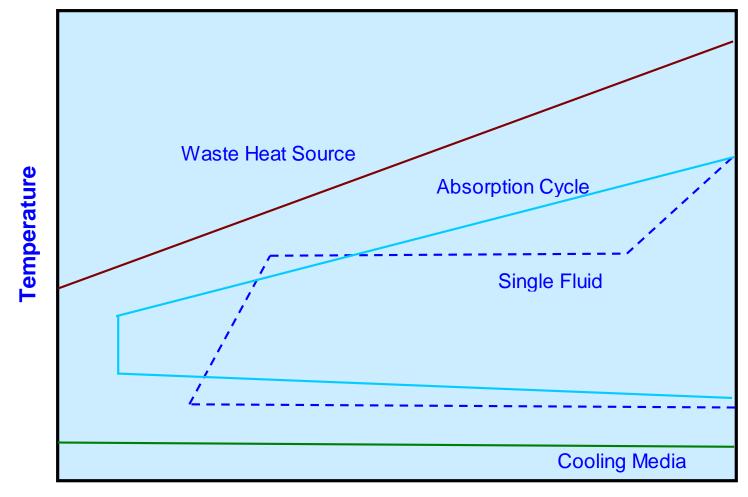
#### Thermal efficiency should be based on total recoverable waste heat

$$\eta_{WH} = \frac{\text{Cycle Efficiency Based on Heat Recoverd}}{\text{Carnot Efficiency}}$$



### **Conversion Efficiency and Effective Utilization of Waste Heat**

Impact of Heat Transfer Performance on Cycle Efficiency





# Heat Transfer Equipment

- Waste heat source to the cycle
  - Corrosion and material considerations
  - Fouling: severity, mitigation, monitoring, cleaning
- Internal heat transfer equipment
  - Numbers and complexity
  - Design constraints and impact on cycle performance
- Heat rejection exchanger
  - Availability of cooling water or make-up water for evaporative coolers/condenser
  - Dry cooling

## System integration and interfacing with industrial processes

- Interfacing of waste heat source to the cycle: space, accessibility, interfacing piping, impact on the process unit, need for a closed loop to transfer waste heat to power cycle
- Heat rejection: Integrated with the plant cooling system or independent system, availability of make-up water or dry cooling
- Power system integration and controls
- Maintenance requirements that would impact system integration
- Availability of Space for the Power System



System reliability

- Validated performance of individual components
- Validated performance of the prototype power system
- Dynamic performance of the power system that may impact industrial processes
- Impact of fouling of waste heat recovery heat transfer equipment on the system performance
- Inherent safety measures for ammonia and hydrocarbon systems



- Cost of electricity (COE): present and projected COE over the life of the waste heat to power system
- Combined power and refrigeration: value of refrigeration on energy efficiency as well as improved productivity
- Productivity improvements
- Environmental benefits



- Step 1: Determine incentives: Just COE or end-use benefits (refrigeration, operating rotating equipment, expanding capacity)
- Step 2: Characterize the waste heat source and evaluate technical issues of interfacing with the power system
- Step 3: Use technology merit criteria to screen different power cycles, including combined cycles, and down select to two (may be three) options
- Step 4: Perform a conceptual design to identify major technical issues, and possibly down select to one option
- Step 5: Preliminary design with planning-stage cost estimates based on budgetary quotes of components and subsystems
- Step 6: Decision to go forward with the installation of the waste heat to power system

Perspectives Waste heat – a hidden source of energy

- Significant loss of thermal energy from furnace/fired heater/boiler stack gases and calciners & driers
- Significant low-level (150F to 250F) energy is lost to cooling towers in the form of latent heat from overhead condensers in distillation
- Low pressure steam a major source of waste heat
- Lack of incentives, such as GHG emission credits
- Lack of design/economic tools to evaluate effective utilization of recovered process waste heat in *High-Value* applications – power, refrigeration, heat pumping
- Process heat recovery must be applied to existing plants, with uncertain costs of retrofitting
- Major technical barriers of fouling and corrosion of waste heat sources
  - Scarcity of fresh water in some regions for heat rejection